

# High-Loading Composition-Tolerant Co–Mn Spinel Oxides with Performance beyond 1 W/cm<sup>2</sup> in Alkaline Polymer Electrolyte Fuel Cells

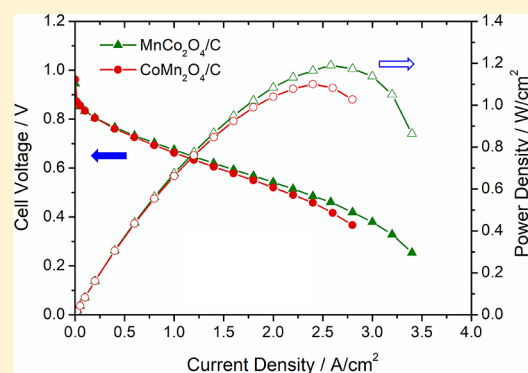
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## Supporting Information

**ABSTRACT:** Hydrogen fuel cells operated in alkaline media enable the use of abundant nonprecious 3d metal oxides to replace Pt to catalyze the sluggish oxygen reduction reaction (ORR). Herein, we describe Co–Mn spinel oxide electrocatalysts with metal oxide loadings of up to 80 wt % on carbon supports. Despite little variation in ORR activity derived from rotating disk electrode (RDE) measurements, practical membrane electrode assembly (MEA) tests exhibited significant enhancement in performance when loadings increased from 40 to 80 wt %. This was ascribed to the enhanced mass transport through the thin catalyst layer at 80 wt % (<10 μm). This work highlights the importance of incorporating MEA tests, even in early-stage catalyst development. A benchmark peak power density (PPD) of 1.2 W/cm<sup>2</sup> at 2.6 A/cm<sup>2</sup> was achieved using MnCo<sub>2</sub>O<sub>4</sub> (80 wt %). CoMn<sub>2</sub>O<sub>4</sub>/C also achieved a PPD of 1.1 W/cm<sup>2</sup> under the same conditions, indicating that MEA performance of Co–Mn oxides is generally high and tolerant to compositional variations that may occur in larger-scale production.



Hydrogen fuel cells have been recognized as a critical renewable energy technology, especially for powering electric vehicles (EVs).<sup>1–3</sup> Despite the tremendous effort in lowering Pt loading in the cathode of proton-exchange membrane fuel cells (PEMFCs), a significant amount of Pt (>0.2 g<sub>Pt</sub>/kW) is still necessary to provide a power density of >1 W/cm<sup>2</sup> at ≥0.65 V, and the catalyst cost accounts for more than 1/3 of a PEMFC stack cost.<sup>4–8</sup> Alternatively, alkaline polymer electrolyte fuel cells (APEFCs) or anion-exchange membrane fuel cells (AEMFCs), in principle, enable the use of nonprecious metals or metal oxides as stable ORR electrocatalysts.<sup>9,10</sup> A variety of candidates have been reported to show promising ORR activity in alkaline media from rotating disk electrode (RDE) tests, such as precious metal-based alloys,<sup>11–13</sup> N-doped carbons,<sup>14,15</sup> and 3d transition metal oxides.<sup>16–24</sup> However, only few have demonstrated encouraging membrane electrode assembly (MEA) performance in alkaline media.<sup>18,19</sup>

In the development of PEMFCs and APEFCs, the RDE has been widely used in research laboratories to screen electrocatalysts and evaluate their activity/durability. For example, RDE measurements showed rather good quantitative agree-

ment with MEA tests for the benchmark activities of Pt/C in PEMFCs.<sup>3</sup> However, RDE and MEA measurements have significant differences in terms of the test conditions, water management, mass transport mechanism, etc. For instance, although spectacular ORR activity of shape-controlled Pt-based alloy catalysts, up to a factor of 20 relative to Pt/C, was reported from RDE measurements,<sup>25–29</sup> those reports have not translated into realistic MEA results in PEMFCs. After only 1 day of MEA testing, octahedral PtNi catalysts exhibited a loss of their distinct shapes and leached out a significant amount of Ni, contaminating the membrane.<sup>4</sup> In other RDE studies, it was shown that 1–3 atomic layers of Pt on the surface of Pt-based alloys yielded the highest ORR activity under acidic conditions.<sup>8,29–31</sup> However, MEA results in PEMFCs suggested that 4–7 atomic layers of Pt were required to effectively mitigate the transition metal leaching problem while still being thin enough to maintain the lattice strain for enhanced activities.<sup>32–34</sup> In our previous study on

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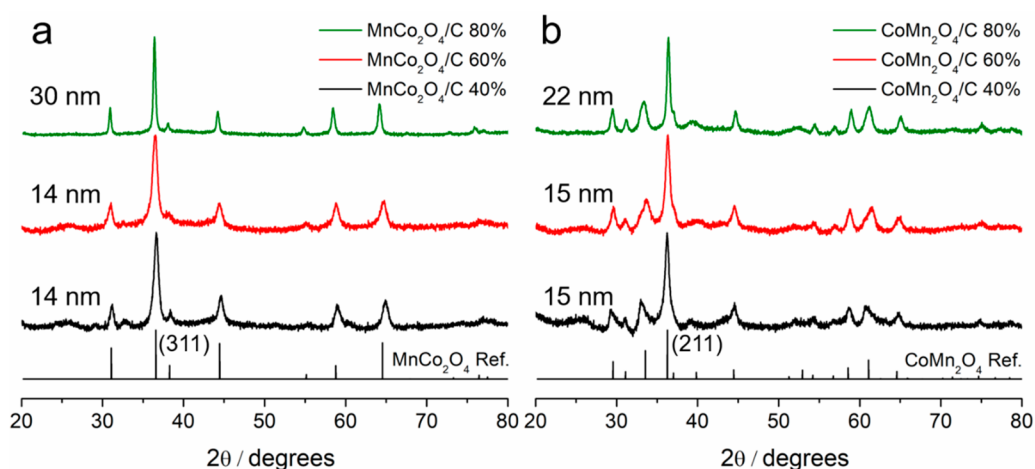


Figure 1. Powder XRD patterns of (a)  $\text{MnCo}_2\text{O}_4$  and (b)  $\text{CoMn}_2\text{O}_4$  NPs with 40, 60, and 80 wt % metal oxide loadings on high-surface-area carbon HSC KB, compared to XRD references of spinel-type  $\text{MnCo}_2\text{O}_4$  and  $\text{CoMn}_2\text{O}_4$ . Domain sizes of  $\text{MnCo}_2\text{O}_4$  and  $\text{CoMn}_2\text{O}_4$  NPs are listed on the left side of the XRD patterns.

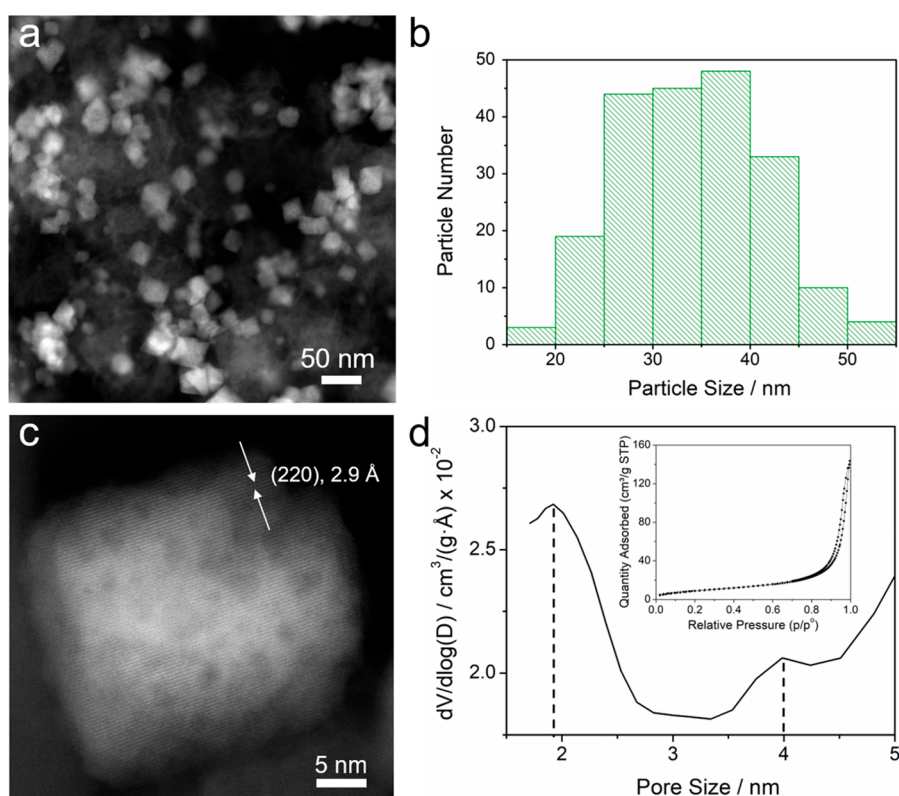


Figure 2. (a) HAADF-STEM image of  $\text{MnCo}_2\text{O}_4$  with 40 wt % metal oxide loading on HSC KB. (b) PSD histogram of  $\text{MnCo}_2\text{O}_4$  NPs. (c) Atomic-scale STEM image of one  $\text{MnCo}_2\text{O}_4$  particle with (220) lattice  $d$ -spacings (2.9 Å). (d) Pore size distribution of  $\text{MnCo}_2\text{O}_4$  without a carbon support, derived from the  $\text{N}_2$  adsorption–desorption isotherm in the inset. The y-axis represents the logarithmic differential pore volume distribution,  $dV/d \log(D)$ , derived from the BJH method. Dashed lines indicate the existence of micropores (1.9 nm) and small mesopores (4.0 nm) in the porous  $\text{MnCo}_2\text{O}_4$  NPs.

$\text{Co}_{1.5}\text{Mn}_{1.5}\text{O}_4/\text{C}$  for APEFCs, only modest activity was observed from RDE measurements. However, a high power density in MEA measurements, surpassing that of Pt/C at lower relative humidity, was achieved by optimizing the surface composition.<sup>18</sup> The RDE–MEA correlation/discrepancy shows that it is important to include MEA tests in early stage catalyst development, in addition to RDE measurements for catalyst screening.

In this work, we reported on Mn–Co spinel oxide electrocatalysts as the oxygen cathode in practical MEA tests in APEFCs.  $\text{MnCo}_2\text{O}_4/\text{C}$  (80 wt %) exhibited a peak power density (PPD) of  $1.2 \text{ W}/\text{cm}^2$ , a benchmark value compared to the state-of-art nonprecious cathodes using N-doped carbon ( $<0.5 \text{ W}/\text{cm}^2$ )<sup>15,35–38</sup> and 3d metal oxides ( $0.5–1 \text{ W}/\text{cm}^2$ ).<sup>18,19</sup> With further optimization on MEA components, we predict that Co–Mn oxides could eventually achieve or surpass the performance of precious metal cathodes (e.g., Pt,

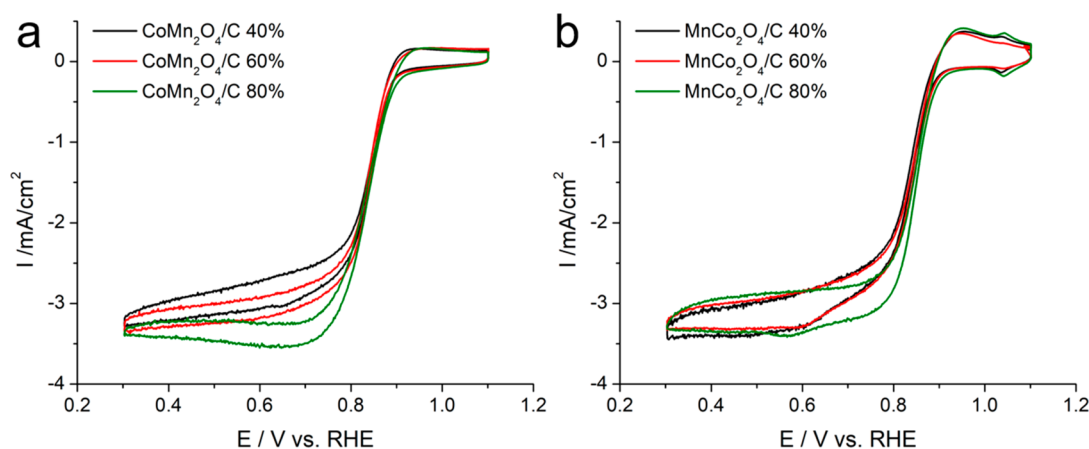


Figure 3. (a) ORR polarization profiles for MnCo<sub>2</sub>O<sub>4</sub> and (b) CoMn<sub>2</sub>O<sub>4</sub> with 40, 60, and 80 wt % metal oxide loading on HSC KB in O<sub>2</sub>-saturated 1 M KOH at a rotation rate of 1600 rpm and a scan rate of 5 mV/s with a catalyst loading of 0.25 mg/cm<sup>2</sup>.

Pd-, and Ag-based catalysts) in APEFCs (1.0–1.5 W/cm<sup>2</sup>).<sup>13,14,39–44</sup> The MEA measurements in the literature are summarized in Table S1.

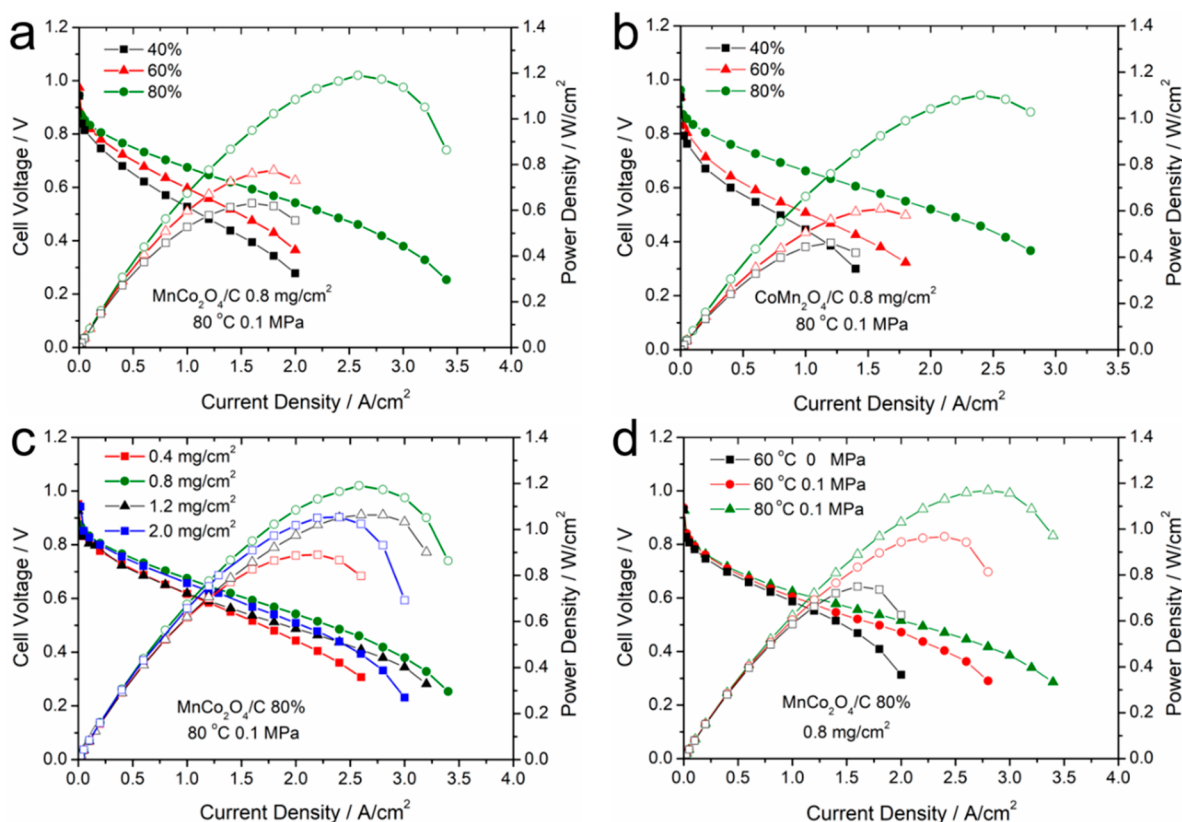
MnCo<sub>2</sub>O<sub>4</sub> and CoMn<sub>2</sub>O<sub>4</sub> nanoparticles (NPs) were synthesized using a facile hydrothermal method, using an autoclave, with various metal oxide loadings on carbon supports (Figure S1). Briefly, metal precursors were reacted with ammonium hydroxide to form coordination compounds, which gradually produced metal hydroxide precipitation from the solution through an aging process, at controlled temperatures with selected solvents. Metal hydroxides finally formed spinel metal oxide NPs, supported on high-surface-area carbon Ketjen black (HSC KB) with desired mass loadings. In general, the pH and ethanol/H<sub>2</sub>O volume ratio of the solvent control the precipitation rate of metal hydroxides, and therefore, those influence the final metal oxide particle size, morphology, and distribution on the carbon substrate. HSC KB has a mesoporous structure and a large Brunauer–Emmett–Teller (BET) surface area of 900 m<sup>2</sup>/g, which was proved to be a better carbon support than the solid carbon, Vulcan XC-72, with a BET surface area of 250 m<sup>2</sup>/g in early reports in PEFMCs.<sup>4</sup> Crystal structures of MnCo<sub>2</sub>O<sub>4</sub>/C and CoMn<sub>2</sub>O<sub>4</sub>/C were examined using powder X-ray diffraction (XRD) (Figure 1). MnCo<sub>2</sub>O<sub>4</sub>/C with metal oxide loadings of 40, 60, and 80 wt % all exhibited single-phase cubic spinel structures when compared to the MnCo<sub>2</sub>O<sub>4</sub> reference (Figure 1a). Such a high loading of 80 wt % has not been reported before for the oxygen cathode in hydrogen fuel cells, although it is a common value used for fabricating the metal oxide cathodes in Li-ion batteries.<sup>45</sup> Average domain sizes of 40, 60, and 80 wt % MnCo<sub>2</sub>O<sub>4</sub>/C were calculated to be 14, 14, and 30 nm, respectively, using the major (311) peak based on the Scherrer equation. Larger domain sizes of 80 wt %, relative to 40 and 60 wt %, suggested that nanocrystals could grow into a larger size at a higher coverage of metal oxides on carbon. As a comparison, CoMn<sub>2</sub>O<sub>4</sub>/C, with various metal oxide loadings, showed a single-phase tetragonal spinel structures due to the strong Jahn–Teller effect of Mn (Figure 1b). The domain size of 80 wt % CoMn<sub>2</sub>O<sub>4</sub>/C was calculated to be 22 nm using the (211) major diffraction peak (PDF # 01-077-0471), which was slightly larger than those at 40 and 60 wt % (15 nm).

The microstructure of Co–Mn NPs supported on HSC KB was examined using aberration-corrected high-angle annular dark-field (HAADF) scanning transmission electron micros-

copy (STEM). As shown in Figure 2a, MnCo<sub>2</sub>O<sub>4</sub> NPs (40 wt %) with an octahedral morphology were well-embedded in the carbon matrix. Particle size distribution (PSD) histograms exhibited an average size of 35 nm (Figure 2b), indicating that the majority of the MnCo<sub>2</sub>O<sub>4</sub> NPs have several subdomains, given the XRD domain size of 14 nm. Atomic-scale STEM images further showed the internal structure of individual MnCo<sub>2</sub>O<sub>4</sub> NPs. As shown in Figures 2c and S2, single-crystal MnCo<sub>2</sub>O<sub>4</sub> particles showed lattice *d*-spacings of 2.9 Å, which matched the theoretical value, 2.93 Å, of MnCo<sub>2</sub>O<sub>4</sub> (220) reflection (PDF # 01-084-0482). Because the STEM image intensity is proportional to the atomic number and relative atomic density, the variation in image contrast suggests the existence of nm-sized pores.

To quantify the porosity of MnCo<sub>2</sub>O<sub>4</sub> without the influence of the mesoporous carbon substrate, MnCo<sub>2</sub>O<sub>4</sub> metal oxides were also synthesized without adding HSC KB. The pore size distribution was derived from the N<sub>2</sub> adsorption–desorption isotherm using the Barrett–Joyner–Halenda (BJH) method (Figure 2d). It shows major micropores of 1.9 nm as well as minor small mesopores of 4.0 nm, which are consistent with the pore sizes indicated from previous STEM images (Figures 2c and S2). The specific surface area was estimated to be 34 m<sup>2</sup>/g based on the BET analysis (Figure 2d, inset). The electrical conductivity of porous MnCo<sub>2</sub>O<sub>4</sub>, without a carbon support, was estimated to be 19 mS/m when compared to typical values of Si (1.6 mS/m) and amorphous carbon (10<sup>2</sup>–10<sup>3</sup> S/m, Figure S3). Given the fact that bulk MnCo<sub>2</sub>O<sub>4</sub> is an insulator with a band gap of 2.11 eV,<sup>46</sup> the electronic conductivity of MnCo<sub>2</sub>O<sub>4</sub> NPs may come from crystal defects and small particle sizes, leading to a smaller ohmic resistance for the ORR. CoMn<sub>2</sub>O<sub>4</sub> NPs (40 wt %) exhibited a similar octahedral morphology with an average particle size of 22 nm, which also indicated the existence of subdomains and nm-sized pores, given the XRD domain size of 15 nm and the STEM image contrast variation (Figure S4).

After thorough structural examination, the Mn–Co spinel oxides with various metal oxide loadings were employed as electrocatalysts for the ORR in alkaline media. ORR polarization profiles were acquired in O<sub>2</sub>-saturated 1 M KOH at a rotation rate of 1600 rpm and a scan rate of 5 mV/s with a catalyst loading of 0.25 mg/cm<sup>2</sup>. While the metal oxide loadings increased from 40 to 60 and finally 80 wt %, CoMn<sub>2</sub>O<sub>4</sub>/C showed a similar ORR activity with a high half-



**Figure 4.** MEA measurements of AEMFCs using Co–Mn spinel oxides in the cathode, 60 wt % PtRu/C ( $0.4 \text{ mg}_{\text{PtRu}}/\text{cm}^2$ ) in the anode, and QAPTT as the alkaline membrane ( $30 \pm 5 \mu\text{m}$ ) and ionomer binder (20 wt % in the catalyst layers). Fully humidified  $\text{H}_2$  and  $\text{O}_2$  gases were fed into the cell at a flow rate of 1000 mL/min. (a,b) MEA results of  $\text{MnCo}_2\text{O}_4/\text{C}$  and  $\text{CoMn}_2\text{O}_4/\text{C}$  with 40, 60, and 80 wt % metal oxide loadings on HSC KB. The catalyst loadings in the cathode were all controlled to be  $0.8 \text{ mg}_{\text{metal oxide}}/\text{cm}^2$ , and the cell operating conditions were  $80^\circ\text{C}$  with 0.1 MPa back-pressure. (c) MEA results of  $\text{MnCo}_2\text{O}_4/\text{C}$  (80 wt %) with a series of catalyst loadings from 0.4 to  $2.0 \text{ mg}/\text{cm}^2$  in the cathode with operating conditions of  $80^\circ\text{C}$  and 0.1 MPa back-pressure. (d) MEA results of  $\text{MnCo}_2\text{O}_4$  at different operating conditions ( $60$  or  $80^\circ\text{C}$ ; with or without 0.1 MPa back-pressure). Metal oxide loadings on carbon were controlled to be 80 wt %, and catalyst loadings in the cathode were  $0.8 \text{ mg}_{\text{metal oxide}}/\text{cm}^2$ . All of the monotonic cell voltage–current density profiles correspond to the left y-axes, while all of the parabolic power density–current density profiles correspond to the right y-axes.

wave potential ( $E_{1/2}$ ) of around 0.84 V vs RHE and  $\Delta E_{1/2} < 3 \text{ mV}$  (Figure 3a). Noticeable changes appeared only when the potential was lower than 0.8 V vs the reversible hydrogen electrode (RHE).  $\text{CoMn}_2\text{O}_4/\text{C}$  with an 80 wt % metal oxide loading achieved the desired diffusion-limited current density at a more positive potential, relative to samples with 60 and 40% loadings. When compared to  $\text{CoMn}_2\text{O}_4/\text{C}$ ,  $\text{MnCo}_2\text{O}_4$  also exhibited similar ORR activity with changes in  $E_{1/2}$  less than 5 mV as the metal oxide loading increased from 40 to 80 wt % (Figure 3b). Similar improvement in the high-polarization region was also observed at higher loading despite the small differences between 40 and 60 wt %. The minor redox peaks of  $\text{MnCo}_2\text{O}_4$  at 1.05 V were assigned to monolayer active species on the surface with a highly reversible reaction process (Figure S5). The less smooth changes in the current density at around 0.6 V were ascribed to the influence of  $\text{MnCo}_2\text{O}_4$  reduction peaks at 0.6 V (Figure S5). One may conclude that  $\text{MnCo}_2\text{O}_4/\text{C}$  and  $\text{CoMn}_2\text{O}_4/\text{C}$  with high loading (60 and 80 wt %) do not present significant advantages as ORR electrocatalysts, relative to the 40 wt %, which is commonly reported as the metal oxide loading for both RDE and MEA measurements in the literature.<sup>19–24</sup> However, later practical MEA tests of Mn–Co oxides demonstrated the unexpected difference in performance with various metal oxide loadings on carbon (vide infra).

The  $\text{H}_2$ – $\text{O}_2$  cell performance was tested using the quaternary ammonium poly(*N*-methylpiperidine-*co-p*-terphenyl) (QAPPT, IEC = 2.58 mmol/g), which was developed early in our group for stable cell operation at  $80^\circ\text{C}$  as the alkaline membrane (thickness of  $30 \pm 5 \mu\text{m}$ , Figure S6) and ionomer binder in MEA measurements.<sup>40</sup> PtRu/C (60 wt %,  $0.4 \text{ mg}_{\text{PtRu}}/\text{cm}^2$ ) was used as the anode catalyst and Mn–Co spinel oxides as the cathode catalyst. The cell was operated at 60 or  $80^\circ\text{C}$  with or without 0.1 MPa back-pressure. Both  $\text{CoMn}_2\text{O}_4/\text{C}$  and  $\text{MnCo}_2\text{O}_4$  exhibited an impressive enhancement in PPD at  $80^\circ\text{C}$  with 0.1 MPa back-pressure as the metal oxide loading increased from 40 to 80 wt % (Figure 4a,b). The PPD of  $\text{CoMn}_2\text{O}_4/\text{C}$  showed a 2-fold enhancement from  $0.63 \text{ W}/\text{cm}^2$  at 40 wt % to  $1.2 \text{ W}/\text{cm}^2$  at 80 wt %, while the PPD of  $\text{CoMn}_2\text{O}_4/\text{C}$  was also boosted from  $0.46 \text{ W}/\text{cm}^2$  at 40 wt % to  $1.1 \text{ W}/\text{cm}^2$  at 80 wt % (Figure 4a,b and Tables S2 and S3). To the best of our knowledge, this performance of  $>1 \text{ W}/\text{cm}^2$  at a current density of  $>2.5 \text{ A}/\text{cm}^2$  represents the highest PPD ever achieved by nonprecious ORR electrocatalysts in AEMFCs<sup>15,18,19,35–38</sup> and is comparable to the state-of-the-art MEA results of Pt/C (Figure S7). This significant performance enhancement was ascribed to the enhanced mass transport efficiency at higher metal oxide loadings. The catalyst loadings in MEA were fixed at  $0.8 \text{ mg}_{\text{metal oxide}}/\text{cm}^2$ , so that the carbon loadings in MEA were 1.2,

0.53, and 0.20 mg/cm<sup>2</sup> at metal oxide loadings of 40, 60, and 80 wt %, respectively. SEM images of the cross section showed that the thickness of the catalyst layer decreased from 38 at 40 wt % to 16 at 60 wt % and finally to 8 μm at 80 wt % (Figure S6). A thinner catalyst layer of <10 μm at 80 wt % is more efficient for O<sub>2</sub>, H<sub>2</sub>O, and OH<sup>-</sup> transport, which could more effectively supply reactants, especially for high current densities (>2 A/cm<sup>2</sup>), leading to a higher PPD performance.

The impact of the catalyst loading in the cathode was investigated from 0.4 to 2.0 mg<sub>metal oxide</sub>/cm<sup>2</sup> (Figure 4c). The cell PPD performance improved significantly from 0.89 to 1.2 W/cm<sup>2</sup> when the catalyst loadings increased from 0.4 to 0.8 mg/cm<sup>2</sup>, which was attributed to the increased amount of catalyst active sites. However, further increases in the catalyst loading from 0.8 to 2.0 mg/cm<sup>2</sup> resulted in a noticeable decrease in the PPD from 1.2 to 1.0 W/cm<sup>2</sup>. With catalyst loadings higher than 0.8 cm<sup>2</sup>, the mass transport limitation became dominant, relative to the increase in the amount of active sites. Different cell operating conditions were also systematically studied, including cell temperatures and operation with or without back-pressure (Figure 4d). The MEA with MnCo<sub>2</sub>O<sub>4</sub>/C (80 wt %) exhibited a PPD enhancement from 0.92 to 1.0 W/cm<sup>2</sup> by applying a 0.1 MPa back-pressure to both H<sub>2</sub> and O<sub>2</sub> and a further PPD increase from 1.0 to 1.2 W/cm<sup>2</sup> when the temperature increased from 60 to 80 °C with a 0.1 MPa back-pressure. CoMn<sub>2</sub>O<sub>4</sub> showed a similar PPD increase from 0.78 W/cm<sup>2</sup> at 60 °C with no back-pressure to 1.1 W/cm<sup>2</sup> at 80 °C with back-pressure (Figure S8). This suggests that Co–Mn spinel oxides have excellent temperature-tolerant performance at both 60 and 80 °C, which is critical to maintain the high energy efficiency of fuel cells.<sup>2–4</sup> Few precious<sup>14,40</sup> or nonprecious<sup>18</sup> ORR electrocatalysts can work at such a high temperature of 80 °C at a PPD above 1 W/cm<sup>2</sup>. This high power density was attributed to the combination of the high-loading active Co–Mn oxide electrocatalysts and stable QAPPT membrane/ionomers.

In summary, APEFCs with a record peak performance of over 1W/cm<sup>2</sup> power density were achieved for both nonprecious MnCo<sub>2</sub>O<sub>4</sub>/C (1.2 W/cm<sup>2</sup> at 2.6 A/cm<sup>2</sup>) and CoMn<sub>2</sub>O<sub>4</sub>/C (1.1 W/cm<sup>2</sup> at 2.4 A/cm<sup>2</sup>) with a high metal oxide loading of 80 wt % at 80 °C with 0.1 MPa back-pressure. This work suggests that MEA performance of Co–Mn spinel oxides is generally high even as the Co mole fraction of the cations varies from 2/3 to 1/3 from MnCo<sub>2</sub>O<sub>4</sub>/C to CoMn<sub>2</sub>O<sub>4</sub>/C. Consequently, even when Mn–Co oxide NPs have variations in Mn and Co contents after large-scale synthesis, it will be less challenging to achieve the desired performance in practical fuel cell applications.

## ■ ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acseenergylett.9b00597.

Experimental methods, synthesis method, structural characterizations, electrochemical characterizations, MEA tests (PDF)

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\*Y.Y. and H.P. contributed equally to this work.

### Notes

The authors declare no competing financial interest.

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